



DECLARATION

I, Jane Roberta Mann, B.A., a Translator, of Frank B. Dehn & Co., 59 St Aldates, Oxford OX1 1ST, England, do declare that I have a competent knowledge of the English and German languages and that the document that is annexed hereto is a true and accurate translation of the German text of the U.S. Provisional Application Serial No. 60/499,514 filed September 2, 2003.

I further declare that all statements made of my own knowledge are true and that all statements made on information and belief are believed to be true.

I acknowledge that wilful false statements and the like are punishable by fine or imprisonment, or both [18 U.S.C. 1001] and may jeopardize the validity of the application or any patent issuing therefrom.

Signed this 21st day of October, 2003

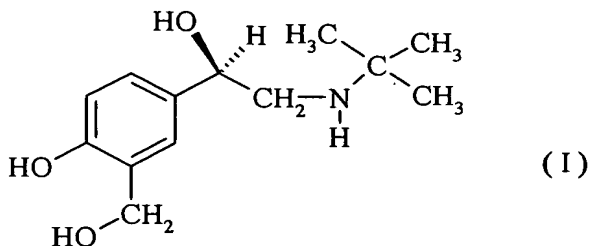
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Process for preparing (R)-salbutamol

The present invention relates to an improved process for preparing (R)-salbutamol by rhodium-catalysed asymmetrical hydrogenation on an industrial scale.

Technical background to the invention

(R)-Salbutamol, levosalbutamol or (R)-albuterol is α -[[[(1,1-dimethylethyl)-amino]methyl-4-hydroxy-1,3-benzenedimethanol, belongs to the β -2-agonists used pharmaceutically as bronchodilators and is of considerable commercial interest. The chemical structure of the chiral α -aminoalcohol (R)-salbutamol is shown in formula I:



Prior art

The methods of preparing (R)-salbutamol known from the prior art include the racemate cleaving of racemic salbutamol using di-toluytartaric acid, e.g. according to US Patent US 5,399,765. In addition, International Patent Application WO 95/29146 proposes the preparation of (R)-salbutamol starting from corresponding alpha-iminoketone by enantioselective reduction with boranes in the presence of a chiral oxaborazole catalyst.

However, the processes described in the prior art are not suitable for preparing (R)-salbutamol on an industrial scale as half the valuable starting product is lost during the racemate cleaving and large amounts of the oxaborazole catalyst, which is difficult to obtain, have to be used during the enantioselective reduction.

One of the primary objectives of the present invention is to develop a process by means of which (R)-salbutamol can be prepared with a high degree of optical and chemical purity. This is intended, for example, to minimise the danger of drugs which contain (R)-salbutamol as active substance being contaminated with the unwanted D-enantiomer.

Another aim of the invention is to develop a process by means of which (R)-salbutamol can easily be prepared in substantially enantiomerically pure form from starting materials which are easily obtained.

Another aim of the invention is to prepare (R)-salbutamol by means of a stereoselective process in order to avoid reaction steps in which chiral intermediate compounds or the chiral end product (R)-salbutamol is obtained as a racemate in a similar amount to the corresponding antipode.

Surprisingly it has now been found that (R)-salbutamol can be obtained on an industrial scale in very good yields and with good optical purity if salbutamone is subjected to asymmetric hydrogenation in the presence of rhodium and a chiral, bidentate phosphine ligand as catalyst system.

Description of the invention

The present invention relates to a process for preparing levosalbutamol or (R)-salbutamol or the pharmacologically acceptable salts thereof starting from prochiral salbutamone as educt, in which salbutamone is subjected to asymmetric hydrogenation in the presence of rhodium and a chiral bidentate phosphine ligand (PP*), particularly (2R, 4R)-4-(dicyclohexylphosphino)-2-(diphenylphosphino-methyl)-N-methyl-aminocarbonyl-pyrrolidine, as catalyst system, and the levosalbutamol obtained is optionally converted into a salt with an acid.

In a preferred process the asymmetric hydrogenation is carried out in a temperature range from 20°C to 100°C, preferably from 40°C to 60°C, particularly from 45°C to 55°C.

Also preferred is a process in which the asymmetric hydrogenation is carried out under a pressure of more than 1 bar to 100 bar, preferably under a pressure of 10 bar to 50 bar, particularly at about 20 bar.

The reaction media used may be both protic solvents - such as e.g. alcohols and/or water or aprotic polar solvents such as e.g. ethers and/or amides or lactams and/or mixtures thereof. Water may optionally be added to all the solvents. The protic solvents used are preferably branched or unbranched C₁-C₈ alkanols. Particularly preferably, lower alcohols such as methanol, ethanol, n-propanol and isopropanol or mixtures thereof are used. Methanol is particularly preferably used as the reaction medium, while the methanol or the other alcohols or solvents may optionally contain water. Suitable aprotic solvents are polar ethers such as for example tetrahydrofuran or dimethoxyethylether or amides such as for example dimethylformamide, or lactams such as for example N-methylpyrrolidone. Preferably, solvents with a slight tendency to flammability are used.

The reaction is preferably carried out in the presence of a base. The base used may be an organic base or an inorganic bases both in solid form and also in the form of solutions, e.g. aqueous solutions. Suitable inorganic bases are basically reacting alkali metal salts or alkali metal hydroxides. Preferably, alkali metal hydrogen carbonates or alkali metal carbonates are used in addition to alkali metal hydroxides. Most preferably, Na₂CO₃, K₂CO₃, LiOH, NaOH, KOH or NaHCO₃ is used.

Suitable organic bases are tertiary amines, particularly tertiary alkyl-amines, tertiary alkyl-aryl-amines or pyridines. Preferably trialkylamines with branched or unbranched C₁ – C₅-alkyl groups are used. Triethylamine or diisopropylethylamine have proved particularly preferable for example. If

desired the reaction may also be carried out in the presence of basic polymers with e.g. tertiary amino functions.

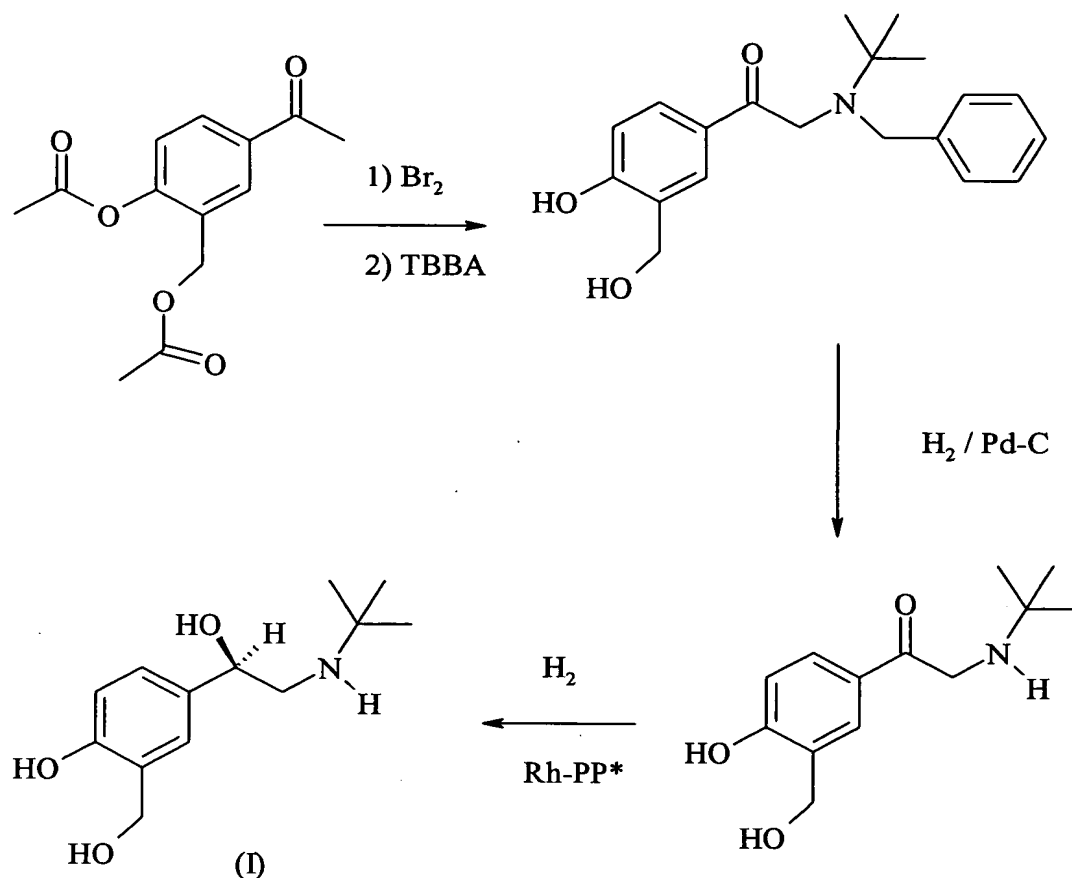
Preferred methods are those wherein salbutamone is used in a molar ratio to the rhodium catalyst of from 500:1 to 100000:1, preferably from 750:1 to 20000:1 during asymmetric hydrogenation.

With a molar ratio of catalyst to substrate of about 1:1000 (R)-salbutamol is obtained in an optical purity of 70 % ee by the process according to the invention starting from salbutamone (reaction plan 1). By converting the salbutamol (I) into an acid addition salt and subsequently precipitating it from an ammonia-methanol-water mixture the optical purity can be further increased in a simple and remarkable manner.

It has also been found that, in contrast to the teaching of WO 95/29146, there is no need to have a molar ratio of catalyst to substrate of about 1:10, as disclosed therein, for the asymmetric reduction in order to obtain good yields or high optical purity. In the process according to the invention this ratio can be drastically lowered by a factor of 10 to 1000. In spite of this significant reduction in the amount of catalyst the (R)-salbutamol resulting from the asymmetric hydrogenation is still obtained in a significantly higher optical yields than by the process known from the prior art. The reduction in the amount of catalyst makes it much easier to purify the product.

By reducing the amount of catalyst and using the commercially favourable salbutamone as educt the costs of producing (R)-salbutamol can be reduced substantially by the new process.

The salbutamone to be used as starting product is obtained by hydrogenation of N-benzylsalbutamone, which may be prepared by brominating 4-acetyloxy-3-acetyloxymethylbenzophenone and subsequently reacting with *tert*-butylbenzylamine (TBBA) according to the following reaction plan:

Reaction plan

In addition, the space-time yield can be improved over that of the prior art using the new process. It is particularly advantageous for preparing (R)-salbutamol on an industrial scale from the point of view of costs and safety.

Finally, it is possible using the process according to the invention to do away with the protection of the phenolic hydroxyl group in salbutamone and still successfully react it to obtain chiral (R)-salbutamol using asymmetric hydrogenation with one of the catalyst systems according to the invention.

According to the invention the catalyst used is $[\text{Rh}(\text{COD})\text{Cl}]_2$, where COD denotes a cyclooctadienyl group, and a chiral, bidentate phosphine ligand (PP*). Preferably (2R, 4R)-4-(dicyclohexylphosphino)-2-(diphenylphosphino-methyl)-N-methyl-aminocarbonylpyrrolidine (RR-MCCPM) is used as catalyst.

The preparation of this catalyst is known from the prior art [EP-A-0 251 164, EP-A-0 336 123]. The catalyst may also be bound to the polymer, e.g. by having the chiral ligand (2R, 4R)-4-dicyclohexylphosphino)-2-(diphenylphosphino-methyl)-N-methyl-aminocarbonyl) pyrrolidine bound to a polymer via the phenyl groups, for example. The use of such polymer-bound ligands does not totally rule out the simultaneous use of non-polymer-bound ligands. Such polymer-bound catalysts are particularly advantageous for simple purification of the product.

The catalyst is either used as a prefabricated, oxygen-free solution of $[\text{Rh}(\text{COD})\text{Cl}]_2$ and ligand or prepared *in situ* from $[\text{Rh}(\text{COD})\text{Cl}]_2$ and ligand in the presence of salbutamone without oxygen in a protective gas atmosphere or hydrogen atmosphere.

The hydrogenation is generally carried out without oxygen, conveniently under inert gas, preferably under a hydrogen atmosphere. However, it is not essential to the reaction that the hydrogen for the hydrogenation should be capable of being taken from the atmospheric gas above the reaction mixture. The hydrogen may also be produced in solution *in situ* from suitable hydrogen sources. Such hydrogen sources include e.g. ammonium formate, formic acid and other formates, hydrazines in the presence of metal ions such as $\text{Fe}^{2+}/\text{Fe}^{3+}$ and other hydrogen sources known from the prior art.

The reaction time for the asymmetric hydrogenation to be completed is generally between 2 and 48 hours, preferably between 4 and 36 hours, and particularly preferably about 23 hours.

The reaction of N-benzyl-salbutamone to obtain salbutamone is carried out by palladium-catalysed hydrogenating debenzylation. The reaction mixture from the asymmetric hydrogenation may be combined with a palladium catalyst without any further working up.

In this method benzyalsbutamone is combined with activated charcoal and a palladium chloride solution and hydrogenated under a pressure of more than 1 to 5 bar, preferably 2 – 3 bar. The further working up is carried out according to methods known from the literature.

The process according to the invention will now be illustrated by the Examples that follow. The skilled man will be aware that the examples are provided solely as an illustration and are not to be viewed as restrictive.

Examples

Example 1 Benzyalsbutamone

900 g of 4-acetyloxy-3-acetyloxymethylbenzophenone are placed in 6 l of suitable solvent. After the addition of 614 g bromine the mixture is refluxed for a further 30 minutes and cooled. After the addition of 1153 g of *tert*-butylbenzylamine the mixture is refluxed for another 20-25 h. After the precipitate has been filtered the organic phase is extracted with hydrochloric acid and the product is crystallised. 806 g of benzyalsbutamone are obtained.

Example 2 Salbutamone

36.4 g of benzyalsbutamone are taken up in 110 ml of water and stirred for 2.5 with 1 g of 10% Pd/C at 2 bar hydrogen pressure and at 40 °C. The precipitate is dissolved with methanol. The solution is filtered through Celite and evaporated down until crystallisation starts. It is cooled overnight to ambient temperature and the crystals are filtered off. After washing with a little cold water and drying overnight at 50 °C in vacuo, salbutamone is obtained in a 92% yield.

Example 3 (R)-(-)-salbutamol

10 g of salbutamone are dissolved in 100 ml of methanol (degassed) and 0.13 ml of triethylamine. 4.7 mg of $(\text{RhCODCl})_2$ and 10 mg of (2R, 4R)-4-dicyclohexylphosphino)-2-(diphenylphosphino-methyl)-N-methyl-aminocarbonyl) pyrrolidine (as a toluenic solution) are added and the mixture is stirred for 23 h at 50 °C and 20 bar hydrogen pressure. The reaction solution is concentrated by rotary evaporation and the residue is recrystallised from ethanol. The salbutamol is obtained in a yield of 90% in an optical purity of approx. 70% e.e.